

THERMODYNAMIC FUNCTIONS FOR 1,4-DICHLORONAPHTHALENE, 1,4-DIBROMONAPHTHALENE AND 2,3-DIBROMONAPHTHALENE FROM 0.25 TO 16 ATMOSPHERES

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ABSTRACT

Real gas thermodynamic functions, C_p , S , $(H - H_0)/T$, and $-(F - H_0)/T$, have been calculated for dihalonaphthalenes (1,4-dichloronaphthalene, 1,4-dibromonaphthalene and 2,3-dibromonaphthalene) from 0.25 atm to 16 atm within the temperature range of 273.15-1200 K, correcting the thermodynamic property ideal gas values by means of the Berthelot equation of state.

INTRODUCTION

McFee and Lielmezs¹⁻³ have calculated the ideal gas state thermodynamic functions at 1 atm for naphthalene and 11 halogenated naphthalenes¹, and the real gas state thermodynamic functions from 0.25 atm to 16 atm for α - and β -halonaphthalenes^{2, 3}, all calculations having been kept within the temperature range 273.15-1200 K. In this work, additionally, real gas thermodynamic functions have been calculated for dihalogenated naphthalenes (1,4-dichloronaphthalene, 1,4-dibromonaphthalene and 2,3-dibromonaphthalene), again from 0.25 to 16 atm and within the temperature range 273.15-1200 K. The calculated results are presented in Table 1. These results have also been fitted to a five-constant polynomial of the form

$$A = a + bT + cT^2 + dT^3 + eT^4 \quad (1)$$

where A is the real gas thermodynamic function in question at temperature T (K). The constants a , b , c , d and e in eqn. (1) have been obtained using linear least-squares curve fitting methods⁴ and are found in Table 2. The molecular structural data needed for thermodynamic function calculations are presented in Table 3.

DISCUSSION

The real gas state thermodynamic properties of dihalogenated naphthalenes

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TABLE I

HEAT CAPACITY $[C_p^0]$, ENTHALPY $[(H^0 \dots H_0^0)/T]$, FREE ENERGY FUNCTIONS $[(F^0 \dots H_0^0)/T]$ AND ENTROPY $[S^0]$, ALL IN UNITS OF CAL. MOL.⁻¹ K⁻¹

Temperature (K)	1,4-Dichloronaphthalene			1,4-Dibromonaphthalene			2,3-Dibromonaphthalene		
	C_p	$(H - H_0)/T$	$-(F - H_0)/T - S$	C_p	$(H - H_0)/T$	$-(F - H_0)/T - S$	C_p	$(H - H_0)/T$	$-(F - H_0)/T - S$
$P = 0.25$ atm									
451.00	55.93	30.78	86.36	56.60	31.83	90.95	56.50	31.63	91.81
522.70	61.59	34.63	91.18	62.13	35.61	95.92	62.07	35.43	96.75
273.15	38.02	19.98	73.79	39.29	21.11	77.82	39.02	20.90	78.78
298.15	40.77	21.60	75.61	41.91	22.74	79.74	41.66	22.53	80.68
300.00	40.97	21.72	75.74	42.10	22.86	79.88	41.85	22.65	80.82
350.00	46.32	24.85	79.33	47.26	25.98	83.64	47.06	25.77	84.55
400.00	51.31	27.86	82.84	52.10	28.95	87.30	51.96	28.74	88.19
450.00	55.84	30.72	86.29	56.51	31.77	90.88	56.41	31.57	91.74
500.00	59.90	33.44	89.67	60.48	34.45	94.37	60.41	34.26	95.20
550.00	63.50	36.01	92.98	64.01	36.98	97.77	63.96	36.80	98.59
600.00	66.70	38.44	96.22	67.15	39.36	101.09	67.12	39.20	101.69
650.00	69.56	40.72	99.38	69.95	41.61	104.33	69.94	41.46	105.12
700.00	72.10	42.88	102.48	72.46	43.73	107.49	72.45	43.58	108.27
750.00	74.39	44.90	105.51	74.71	45.72	110.58	74.71	45.58	111.35
800.00	76.45	46.81	108.47	76.73	47.59	113.59	76.74	47.47	114.35
850.00	78.31	48.61	111.36	78.57	49.36	116.53	78.58	49.24	117.28
900.00	80.00	50.31	114.19	80.23	51.03	119.40	80.24	50.92	120.14
950.00	81.53	51.91	116.95	81.75	52.61	122.20	81.76	52.50	122.94
1000.00	82.94	53.43	119.65	83.13	54.10	124.93	83.14	54.00	125.67
1050.00	84.22	54.86	122.30	84.40	55.51	127.61	84.41	55.42	128.34
1100.00	85.39	56.23	124.88	85.56	56.85	130.22	85.57	56.77	130.95
1150.00	86.47	57.52	127.41	86.62	58.12	132.78	86.64	58.04	133.50
1200.00	87.46	58.74	129.88	87.60	59.33	135.28	87.62	59.25	136.00

$P = 0.50 \text{ atm}$

451.00	56.15	30.67	85.02	115.68	56.85	31.70	89.61	121.31	56.75	31.50	90.47	121.97
522.70	61.73	34.55	89.83	124.38	62.29	35.53	94.57	130.10	62.24	35.35	95.40	130.75
273.15	39.04	19.47	72.58	92.05	40.43	20.54	76.63	97.17	40.17	20.33	77.59	97.92
298.15	41.55	21.22	74.36	95.57	42.79	22.31	78.50	100.81	42.54	22.09	79.45	101.54
300.00	41.74	21.34	74.49	95.83	42.96	22.44	78.64	101.08	42.72	22.22	79.59	101.80
350.00	46.81	24.62	78.03	102.65	47.80	25.71	82.35	108.07	47.61	25.49	83.26	108.76
400.00	51.64	27.70	81.52	109.22	52.46	28.77	85.99	114.76	52.32	28.56	86.87	115.43
450.00	56.07	30.61	84.95	115.56	56.77	31.65	89.54	121.19	56.67	31.44	90.40	121.84
500.00	60.06	33.36	88.32	121.68	60.66	34.36	93.02	127.37	60.59	34.17	93.85	128.02
550.00	63.63	35.95	91.62	127.57	64.15	36.91	96.41	133.32	64.10	36.73	97.23	133.96
600.00	66.80	38.39	94.85	131.25	67.26	39.31	99.73	139.04	67.23	39.14	100.53	139.68
650.00	69.63	40.69	98.02	138.71	70.04	41.57	102.97	144.53	70.02	41.41	103.76	145.17
700.00	72.17	42.85	101.11	143.96	72.52	43.69	106.12	149.82	72.52	43.55	106.90	150.45
750.00	74.44	44.88	104.14	149.02	74.76	45.69	109.21	154.90	74.76	45.56	109.98	155.53
800.00	76.49	46.79	107.10	153.89	76.78	47.57	112.22	159.79	76.78	47.45	112.98	160.43
850.00	78.34	48.59	109.99	158.58	78.60	49.34	115.15	164.50	78.61	49.23	115.91	165.14
900.00	80.03	50.29	112.82	163.11	80.26	51.02	118.02	169.04	80.28	50.91	118.77	169.68
950.00	81.56	51.90	115.58	167.48	81.77	52.60	120.82	173.42	81.79	52.49	121.57	174.06
1000.00	82.96	53.42	118.28	171.70	83.15	54.09	123.56	177.65	83.17	53.99	124.30	178.29
1050.00	84.24	54.86	120.92	175.78	84.42	55.50	126.23	181.74	84.43	55.41	126.97	182.38
1100.00	85.41	56.22	123.50	179.72	85.57	56.85	128.85	185.69	85.59	56.76	129.58	186.33
1150.00	86.48	57.51	126.03	183.54	86.64	58.12	131.40	189.52	86.65	58.03	132.13	190.16
1200.00	87.47	58.74	128.51	187.25	87.62	59.33	133.90	193.23	87.63	59.25	134.62	193.87

$P = 2.00 \text{ atm}$

451.00	57.51	30.00	82.48	112.48	58.37	30.95	87.10	118.05	58.29	30.74	87.96	118.70
522.70	62.60	34.13	87.21	121.33	63.27	35.06	91.97	127.02	63.22	34.87	92.80	127.66
273.15	45.14	16.44	70.82	87.26	47.27	17.15	74.99	92.14	47.09	16.89	75.97	92.86
298.15	46.24	18.89	72.37	91.26	48.04	19.70	76.61	96.31	47.86	19.45	77.57	97.01
300.00	46.34	19.06	72.48	91.54	48.12	19.87	76.73	96.60	47.94	19.62	77.69	97.31
350.00	49.71	23.18	75.74	98.93	51.05	24.11	80.12	104.23	50.90	23.87	81.04	104.91
400.00	53.58	26.74	79.07	105.81	54.64	27.69	83.58	111.28	54.53	27.47	84.47	111.94
450.00	57.43	29.94	82.41	112.35	58.30	30.89	87.03	117.92	58.22	30.68	87.89	118.57
500.00	61.06	32.87	85.72	118.59	61.78	33.81	90.44	124.25	61.72	33.61	91.28	124.89
550.00	64.37	35.59	88.98	124.57	64.98	36.50	93.79	130.29	64.95	36.32	94.61	130.93
600.00	67.38	38.11	92.19	130.30	67.90	39.00	97.07	136.07	67.88	38.83	97.88	136.71
650.00	70.08	40.47	95.33	135.80	70.54	41.32	100.29	141.61	70.54	41.17	101.08	142.25
700.00	72.53	42.67	98.41	141.09	72.93	43.50	103.43	146.93	72.93	43.35	104.21	147.56
750.00	74.73	44.74	101.43	146.17	75.09	45.53	106.50	152.03	75.10	45.40	107.27	152.67
800.00	76.73	46.68	104.38	151.05	77.05	47.44	109.50	156.94	77.06	47.31	110.26	157.58
850.00	78.55	48.50	107.26	155.76	78.83	49.24	112.43	161.67	78.84	49.12	113.19	162.31
900.00	80.20	50.21	110.88	160.30	80.45	50.93	115.29	166.22	80.47	50.81	116.04	166.86
950.00	81.70	51.83	112.84	164.68	81.94	52.52	118.09	170.61	81.95	52.42	118.83	171.25
1000.00	83.08	53.36	115.54	168.90	83.29	54.03	120.82	174.85	83.31	53.93	121.56	175.49
1050.00	84.34	54.81	118.18	172.99	84.54	55.45	123.49	178.94	84.55	55.36	124.23	179.58
1100.00	85.50	56.18	120.76	176.94	85.68	56.80	126.11	182.90	85.69	56.71	126.83	183.54
1150.00	86.57	57.47	123.29	180.76	86.73	58.08	128.66	186.73	86.74	57.99	129.38	187.38
1200.00	87.55	58.71	125.76	184.47	87.70	59.29	131.16	190.45	87.71	59.21	131.88	191.09

TABLE I (continued)

Temperature (K)	1,4-Dichloronaphthalene		1,4-Dibromonaphthalene		2,3-Dibromonaphthalene	
	C_p	$(H^{\circ}-H_0)/T - (F^{\circ}-H_0)/T S$	C_p	$(H^{\circ}-H_0)/T - (F^{\circ}-H_0)/T S$	C_p	$(H^{\circ}-H_0)/T - (F^{\circ}-H_0)/T S$
$P = 4.00$ atm						
451.00	59.32	81.39	60.39	29.96	60.34	86.91
522.70	63.76	86.01	64.57	34.42	64.54	91.63
273.15	53.27	70.77	56.38	12.62	56.31	76.11
298.15	52.49	72.01	55.05	16.22	54.95	77.35
300.00	52.48	72.11	55.00	16.46	54.91	77.45
350.00	53.57	74.99	55.38	21.96	55.28	80.37
400.00	56.17	78.11	57.54	26.26	57.46	83.56
450.00	59.25	81.32	60.34	29.89	60.28	86.84
500.00	62.38	84.55	63.26	33.08	63.23	90.14
550.00	65.37	87.76	66.10	35.95	66.08	93.14
600.00	68.14	90.93	68.76	38.58	68.75	96.63
650.00	70.69	94.04	71.22	41.00	71.22	99.81
700.00	73.01	97.11	73.47	43.24	73.48	102.92
750.00	75.13	100.11	75.53	45.32	75.54	105.96
800.00	77.06	103.05	77.41	47.27	77.43	108.94
850.00	78.82	105.92	79.13	49.09	79.15	111.85
900.00	80.42	108.74	80.71	50.81	80.73	114.70
950.00	81.90	111.49	82.15	52.42	82.17	117.49
1000.00	83.25	114.18	83.48	53.94	83.50	120.21
1050.00	84.49	116.62	84.70	55.38	84.71	122.87
1100.00	85.63	119.40	85.82	56.73	85.84	125.47
1150.00	86.67	121.92	86.85	58.02	86.87	128.02
1200.00	87.64	124.39	87.80	59.24	87.82	130.51
						116.64
						125.85
						88.41
						93.27
						93.61
						102.07
						109.58
						116.51
						123.01
						129.17
						135.04
						140.64
						146.00
						151.14
						156.08
						160.83
						165.40
						169.80
						174.01
						178.15
						182.12
						185.96
						189.68

$P = 8.00 \text{ atm}$

451.00	62.93	27.33	80.58	107.91	64.44	27.96	85.31	113.27	64.44	27.71	86.18	113.90
522.70	66.08	32.43	84.99	117.42	67.17	33.15	89.82	122.97	67.17	32.93	90.66	123.59
273.15	69.54	4.31	72.06	76.37	74.60	3.56	76.72	80.27	74.76	3.13	77.75	80.88
298.15	65.00	9.58	72.67	82.25	69.06	9.26	77.29	86.55	69.14	8.88	78.29	87.17
300.00	64.76	9.92	72.73	82.65	68.75	9.63	77.34	86.97	68.83	9.25	78.34	87.59
350.00	61.30	17.44	74.86	92.30	64.04	17.67	79.47	97.14	64.05	17.35	80.42	97.77
400.00	61.35	22.91	77.56	100.47	63.34	23.40	82.22	105.62	63.34	23.11	83.13	106.24
450.00	62.89	27.25	80.52	107.77	64.41	27.88	85.25	113.13	64.41	27.63	86.12	113.75
500.00	65.03	30.92	83.59	114.51	66.23	31.62	88.38	120.01	66.23	31.40	89.23	120.63
550.00	67.36	34.13	86.69	120.82	68.33	34.86	91.55	126.42	68.34	34.66	92.38	127.04
600.00	69.68	37.00	89.78	126.78	70.48	37.74	94.71	132.45	70.50	37.56	95.52	133.08
650.00	71.90	39.60	92.85	132.44	72.57	40.34	97.84	138.18	72.59	40.17	98.64	138.81
700.00	73.98	41.98	95.87	137.85	74.55	42.72	100.92	143.63	74.58	42.56	101.70	144.26
750.00	75.91	44.18	98.84	143.02	76.41	44.90	103.94	148.84	76.43	44.76	104.71	149.47
800.00	77.70	46.22	101.76	147.98	78.14	46.92	106.90	153.83	78.16	46.79	107.67	154.46
850.00	79.36	48.12	104.62	152.74	79.74	48.81	109.80	158.61	79.76	48.68	110.56	159.24
900.00	80.88	49.90	107.42	157.32	81.22	50.57	112.64	163.21	81.24	50.45	113.39	163.85
950.00	82.28	51.56	110.16	161.73	82.59	52.22	115.42	167.64	82.61	52.11	116.17	168.28
1000.00	83.58	53.13	112.85	165.98	83.85	53.77	118.14	171.91	83.87	53.67	118.88	172.55
1050.00	84.77	54.61	115.48	170.09	85.02	55.23	120.80	176.03	85.04	53.13	121.53	176.67
1100.00	85.87	56.01	118.05	174.06	86.10	56.61	123.40	180.01	86.12	56.52	124.13	180.65
1150.00	86.89	57.33	120.57	177.90	87.10	57.91	125.95	183.86	87.12	57.83	126.67	184.50
1200.00	87.83	58.58	123.04	181.62	88.02	59.15	128.44	187.58	88.04	59.07	129.16	188.23

TABLE I (continued)

Temperature (K)	1,4-Dichloronaphthalene		1,4-Dibromonaphthalene		2,3-Dibromonaphthalene	
	C_p	$(H^{\circ}-H_0)/T^{\circ}$	C_p	$(H^{\circ}-H_0)/T^{\circ}$	C_p	$(H^{\circ}-H_0)/T^{\circ}$
$P = 16.0$ atm						
451.00	70.16	23.78	80.35	104.13	72.54	23.98
522.70	70.73	30.16	84.34	114.49	72.37	30.60
573.15	102.08	11.85	76.00	64.15	111.04	14.56
598.15	90.02	2.84	75.37	72.53	97.08	4.66
600.00	89.32	2.27	75.36	73.08	96.26	4.03
650.00	76.77	9.79	75.98	85.77	81.37	9.09
700.00	71.71	17.79	77.85	95.64	74.95	17.66
750.00	70.17	23.68	80.30	103.97	72.56	23.87
800.00	70.34	28.32	83.04	111.36	72.17	28.71
850.00	71.35	32.19	85.92	118.11	72.80	32.68
900.00	72.75	35.51	88.87	124.38	73.92	36.07
950.00	74.31	38.43	91.83	130.26	75.28	39.03
1000.00	75.91	41.05	94.78	135.83	76.72	41.67
1050.00	77.48	43.43	97.69	141.12	78.17	44.06
1100.00	79.00	45.60	100.56	146.17	79.59	46.23
1150.00	80.44	47.61	103.39	151.00	80.95	48.24
1200.00	81.79	49.47	106.16	155.64	82.24	50.09
1250.00	83.06	51.21	108.89	160.09	83.45	51.81
1300.00	84.24	52.83	111.55	164.38	84.59	53.42
1350.00	85.35	54.35	114.17	168.52	85.66	54.93
1400.00	86.37	55.78	116.73	172.51	86.65	56.35
1450.00	87.33	57.13	119.24	176.38	87.58	57.69
1500.00	88.22	58.41	121.70	180.11	88.45	58.96
1550.00						
1600.00						
1650.00						
1700.00						
1750.00						
1800.00						
1850.00						
1900.00						
1950.00						
2000.00						
2050.00						
2100.00						
2150.00						
2200.00						
2250.00						
2300.00						
2350.00						
2400.00						
2450.00						
2500.00						
2550.00						
2600.00						
2650.00						
2700.00						
2750.00						
2800.00						
2850.00						
2900.00						
2950.00						
3000.00						

TABLE 2

CALCULATED CONSTANTS a , b , c , d AND e IN EQN. (1)

Pressure (atm)

A. 1,4-Dichloronaphthalene

	C_p				
	a	b	$c \times 10^3$	$d \times 10^7$	$e \times 10^{11}$
0.25	-5.06558	0.19826	-0.16811	0.57045	-0.92124
0.50	-0.26267	0.17478	-0.12506	0.32499	0.09599
1.00	9.34374	0.12783	-0.03893	-0.36605	2.13090
2.00	28.55632	0.03393	0.13332	-1.74805	6.20036
4.00	66.98050	-0.15387	0.47780	-4.51189	14.33874
8.00	143.8327	-0.52949	1.16683	-10.04033	30.61833
16.00	247.5320	-1.28070	2.54481	-21.09631	63.17413

 $-(F - H_0)/T$

	a	$b \times 10$	$c \times 10^2$	$d \times 10^8$	$e \times 10^{11}$
0.25	52.87711	0.79790	-0.10948	-0.37749	0.17104
0.50	52.29250	0.75903	-0.03813	-0.95018	0.33971
1.00	52.50105	0.68128	0.10465	-2.09640	0.67735
2.00	54.29585	0.52576	0.39023	-4.38884	1.35260
4.00	59.26212	0.21470	0.96126	-8.97258	2.70270
8.00	70.57228	-0.40725	2.10338	-18.14066	5.40316
16.00	94.56909	-1.65119	4.38742	-36.47466	10.80318

 $(H - H_0)/T$

	a	$b \times 10$	$c \times 10^4$	$d \times 10^8$	$e \times 10^{11}$
0.25	-0.34884	0.82461	-0.28825	-0.39783	0.41174
0.50	-2.74291	0.94174	-0.50319	1.32696	-0.09620
1.00	-7.53073	1.17598	-0.93300	4.77601	-1.11191
2.00	-17.10756	1.64454	-1.79293	11.67612	-3.14402
4.00	-36.25911	2.58150	-3.51206	25.47184	-7.20656
8.00	-74.56635	4.45575	-6.95136	53.07234	-15.33507
16.00	-151.1715	8.20356	-13.82821	108.255	-31.58549

S

	a	b	$c \times 10^4$	$d \times 10^8$	$e \times 10^{11}$
0.25	52.52809	0.16225	-0.39775	-0.77521	0.58276
0.50	49.54965	0.17008	-0.54129	0.37654	0.24360
1.00	44.97041	0.18572	-0.82832	2.67927	-0.43441
2.00	37.18875	0.21703	-1.40250	7.28617	-1.79099
4.00	23.00304	0.27963	-2.55081	16.49953	-4.50401
8.00	-3.99098	0.40483	-4.84743	34.92626	-9.93007
16.00	-56.60272	0.65524	-9.44085	71.78111	-20.78253

B. 1,4-Dibromonaphthalene

	C_p				
	a	b	$c \times 10^3$	$d \times 10_1$	$e \times 10^{11}$
0.25	-1.60320	0.18593	-0.14904	0.53215	-0.53961
0.50	3.77721	0.15963	-0.10081	0.14514	0.59998
1.00	14.53819	0.10704	-0.00433	-0.62894	2.87935
2.00	36.06052	0.00185	0.18863	-2.17715	7.43834
4.00	79.10579	-0.20854	0.57456	-5.27360	16.55631
8.00	165.1921	-0.62928	1.34635	-11.46590	34.79035
16.00	337.3684	-1.47080	2.88999	-23.85109	71.26033

TABLE 2 (continued)

Pressure (atm)					
$-(F - H_0)/T$					
	<i>a</i>	<i>b</i> × 10	<i>c</i> × 10 ⁴	<i>d</i> × 10 ⁸	<i>e</i> × 10 ¹¹
0.25	0.58102	0.84589	-0.35196	0.17880	0.23378
0.50	-2.10156	0.97712	-0.39277	2.11122	-0.33531
1.00	-7.46619	1.23956	-1.07430	5.97516	-1.47317
2.00	-18.19701	1.76454	-2.03764	13.70589	-3.74992
4.00	-39.65651	2.81434	-3.96388	29.16278	-8.30166
8.00	-82.57599	4.91400	-7.81655	60.07901	-17.40627
16.00	-168.4168	9.11341	-15.52207	121.9119	-35.61540
$(H - H_0)/T$					
	<i>a</i>	<i>b</i> × 10	<i>c</i> × 10 ⁴	<i>d</i> × 10 ⁸	<i>e</i> × 10 ¹³
0.25	55.26588	0.88277	-0.21727	0.31924	-0.72692
0.50	54.7774	0.83920	-0.13729	-0.32273	18.17952
1.00	55.17790	0.75207	0.02269	-1.60690	56.00358
2.00	57.35649	0.57777	0.34270	-4.17563	131.6639
4.00	63.09090	0.22921	0.98268	-9.31264	282.9693
8.00	75.93867	-0.46904	2.26291	-19.58954	585.6822
16.00	103.0089	-1.86234	4.92284	-40.13748	1190.884
<i>S</i>					
	<i>a</i>	<i>b</i> × 10	<i>c</i> × 10 ⁴	<i>d</i> × 10 ⁸	<i>e</i> × 10 ¹³
0.25	55.26588	0.88277	-0.21727	0.31924	-0.72692
0.50	52.67624	1.81630	-0.72999	1.78775	-15.32358
1.00	47.71114	1.99167	-1.05171	4.36931	-91.35060
2.00	39.15916	2.34234	-1.69499	9.53031	-243.3435
4.00	23.43484	3.04351	-2.98112	19.84449	-547.1784
8.00	-6.63981	4.44613	-5.55407	40.49389	-1155.105
16.00	-65.4109	7.25128	-10.69973	81.77953	-2370.819
<i>C. 2,3-Dibromonaphthalene</i>					
<i>C_p</i>					
	<i>a</i>	<i>b</i>	<i>c</i> × 10 ³	<i>d</i> × 10 ⁷	<i>e</i> × 10 ¹¹
0.25	-2.483980	0.1890391	-0.1530041	0.5538795	-0.5622517
0.50	2.962775	0.1624179	-0.1041716	0.1620785	0.5714625
1.00	13.85629	0.1091756	-0.0065063	0.6215271	2.878904
2.00	35.64401	0.0026856	0.1888381	-2.188885	7.494336
4.00	79.21877	-0.2102894	0.5795124	-5.323444	16.72456
8.00	166.3656	-0.6362184	1.360807	-11.59196	35.1829
16.00	340.6704	-1.488164	2.92363	-24.13157	72.10914
$-(F - H_0)/T$					
	<i>a</i>	<i>b</i> × 10	<i>c</i> × 10 ⁴	<i>d</i> × 10 ⁸	<i>e</i> × 10 ¹²
0.25	56.54803	0.8663541	-0.1966534	0.1916614	0.2383302
0.50	56.07050	0.8222568	-0.1156993	-0.458048	2.151901
1.00	56.49339	0.7340217	0.0462995	-1.758424	5.981887
2.00	58.71620	0.5575763	0.3702517	-4.358732	13.64078
4.00	64.53960	0.2046604	1.018211	-9.559864	28.96033
8.00	77.56296	-0.5011096	2.313966	-19.96039	59.59294
16.00	104.9895	-1.912822	4.905909	-40.76595	120.8743

TABLE 2 (continued)

Pressure (atm)					
	$(H - H_0)/T$				
	a	$b \times 10$	$c \times 10^4$	$d \times 10^8$	$e \times 10^{11}$
0.25	0.5262215	0.8336449	-0.3215286	-0.8931202	0.3156192
0.50	-2.189636	0.9665096	-0.565331	18.67157	-0.2605558
1.00	-7.620900	1.232204	-1.052851	57.79253	-1.412622
2.00	-18.48347	1.763598	-2.027895	136.9345	-3.716744
4.00	-40.20947	2.826445	-3.978116	292.5313	-8.325361
8.00	-83.55006	4.952063	-7.878472	605.5255	-17.54304
16.00	-170.5600	9.203175	-15.67872	1231.448	-35.97547
	S				
	a	b	$c \times 10^4$	$d \times 10^8$	$e \times 10^{11}$
0.25	57.07390	0.1700024	-0.5182411	0.1029281	0.3392538
0.50	53.88126	0.1788733	-0.6809413	1.408112	-0.0450000
1.00	48.87277	0.1966203	-1.006487	4.020139	-0.814167
2.00	40.23260	0.232118	-1.657655	9.244786	-2.352651
4.00	24.32994	0.3031125	-2.959988	19.69445	-5.429883
8.00	-6.096951	0.4450924	-5.56438	40.59023	-11.58285
16.00	-65.57256	-0.1912822	-4.905909	-40.76595	12.08743

were calculated in the same way as those for α - and β -halonaphthalenes^{2, 3}, that is, the already calculated ideal gas state thermodynamic function values for dihalogenated naphthalenes¹ were corrected by means of the second virial coefficient expansion of the Berthelot equation of state^{2, 3}. The resulting equations, given as the real gas deviations from the ideal gas state (at one atmosphere pressure) are^{2, 5}

$$(H - H_0)/T = \frac{9}{128} \frac{RT_c}{P_c} \left[1 - 18 \left(\frac{T_c}{T} \right)^2 \right] P \quad (2)$$

$$(C_p - C_p^0) = \frac{81}{32} \left(\frac{RT_c^3}{P_c T^3} \right) P \quad (3)$$

$$(S^0 - S) = \frac{27}{32} \left(\frac{RT_c^3}{P_c T^3} \right) P + R \ln P \quad (4)$$

The term $R \ln P$ [eqn. (4)] is a correction factor which must be included to obtain the ideal gas entropy at pressure P , provided that this correction term has not already been included in the ideal gas S^0 -expression. The free energy function (Table 1) however is found by subtracting eqn. (4) from eqn. (2). The applicability of the second virial coefficient-truncated Berthelot state equation [eqns. (2-4)] has been discussed in detail by Butler and Lielmezs⁵ for fluorobenzene, and by McFee and Lielmezs^{2, 3} for α - and β -halonaphthalenes. The critical point properties (T_c , P_c) needed for 1,4-dichloronaphthalene were estimated by means of the Lydersen

TABLE 3

MOLECULAR PARAMETERS

	<i>1,4-Dichloronaphthalene</i>				<i>1,4-Dibromonaphthalene</i>				<i>2,3-Dibromonaphthalene</i>						
Fundamental frequencies ^a (ν , cm^{-1})	188	150	224	371	411	185	140	215	371	409	174	139	249	357	406
	494	517	530	597	676	470	517	527	560	662	481	574	593	607	635
	755	745	826	790	816	753	745	823	791	814	738	745	784	814	852
	328	900	824	926	120	289	905	823	927	95	132	878	890	937	294
	956	987	987	1023	224	956	963	963	1021	174	890	947	961	1019	139
	1146	1163	443	1205	1184	1142	1161	377	1207	1187	1136	1148	357	1192	1198
	1260	1371	1363	1371	1415	1256	1368	1352	1368	1410	1262	1338	1301	1418	1428
	1450	1502	1560	1589	1624	1450	1494	1556	1566	243	1476	1576	1556	1383	1624
	3076	328	517	3027	3031	377	3027	3031	3060	3060	3076	279	357	3027	3031
	3060	3060	3076			3076	1624	3076			3060	3060	3076		
Product of the principal moment of inertia ^b ($\text{gm}^2 \text{cm}^6$)															
	2,398,517 $\times 10^{-17}$					10,377,640 $\times 10^{-17}$					9,213,850 $\times 10^{-17}$				
Normal boiling point (K)	563.15					560.00					584.15				
Critical temperature ^c (K)	823.80					859.50					868.00				
Critical pressure ^c (atm)	33.93					34.00					35.00				
Symmetry number (σ)	2					2					2				
Molecular weight	197.07					285.97					285.97				

^a Frequencies selected by McFee and Lielmezs¹.^b Principal moments of inertia calculated by McFee and Lielmezs¹.^c Estimated, this work.

method⁶ using the experimentally-known boiling point⁷ corrected to one atm pressure. However, the critical properties of 1,4-dibromonaphthalene and 2,3-dibromonaphthalene were estimated by analogy with 1,4-dichloronaphthalene as well as with the chlorinated naphthalenes^{2, 3} and benzenes⁸. The error introduced in the critical parameter values will not exceed $\pm 2.0\%$ since the molecular weights of 1,4-dibromonaphthalene and 2,3-dibromonaphthalene are the same; the critical parameters of 1,4-dichloronaphthalene were estimated on the basis of an experimentally-available boiling point temperature value.

The accuracy of the results presented in Tables 1 and 2, and the range of applicability of eqns. (2-4), however, must be inferred from previously discussed² general considerations. Using the error estimation methods already introduced^{1-3, 5} it is found that the calculated ideal gas state thermodynamic functions for dihalogenated naphthalenes should be reliable within the 400-1000 K temperature range 400-1000 K, with the expected error ranging from $\pm 0.5\%$ to $\pm 2\%$.

Indeed, following the error analysis as outlined by McFee and Lielmezs^{2, 3} for real gas thermodynamic function values of α - and β -halonaphthalenes, it is suggested that the calculated real gas thermodynamic function values for dihalogenated naphthalenes (Tables 1 and 2) should not exceed the overall error estimate of $\pm 1\%$ to $\pm 2.5\%$. This error is expected to hold for all pressures between temperatures of 500 and 1100 K. However, it should be noted that thermodynamic properties of any dihalogenated naphthalene gas are determined from their boiling points up. Hence, calculated thermodynamic property values (Tables 1 and 2) should be used noting this limitation. If, however, any thermodynamic property value is used below the boiling point, then such a value would refer to a hypothetical vapor of the dihalogenated naphthalene. This effect starts to become noticeable at pressures higher than 4 atm (Table 1).

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